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Electroformation of quasi-two-dimensional silver patterns in the absence of supporting electrolyte

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Abstract Quasi-two-dimensional (2D) growth patterns of silver electrodeposits obtained from aqueous silver sulfate solution in the absence of supporting electrolyte using a quasi-2D cylindrical cell involve domains with morphologies covering from dense to needle-like branching. The prevailing morphology depends on the electrolyte concentration, applied electric potential and electrolysis time. From the time dependence of the maximum radius circumscribing each electrodeposit, its dimension was obtained. The growth of the solid phase was also analysed in terms of dimensionless numbers to estimate the ionic mass-transfer contributions to the electrochemical process. For a single-growing branch the axial-to-radial growth velocity is close to 10^2 . Phenomena promoting silver electrodeposits with irregular edges and an open structure compete with others operating in the opposite direction. These phenomena are influenced by changes in the concentration and electric potential field around the growing electrodeposit.

Keywords Electrodeposits \cdot Silver \cdot Two-dimensional growth

Introduction

The growth mode of a new solid phase formation depends on the environment, the nature of the substrate including its crystallographic orientation and topography, the temperature, the hydrodynamic conditions and the presence of external fields. The growth mode of the deposit is characterized by its apparent specific gravity and mechanical and surface properties. Random irregularities produced at the growing solid surface by an electric and/ or a concentration field promote local fluctuations favouring the appearance of transitions in the growth mode [1, 2, 3].

Several procedures have been described for the preparation of solid branched aggregates. Among them, electrochemical procedures make it possible to control the quality of metal electrodeposits by handling operating variables over a wide range using either quasi-two-dimensional (2D) [4, 5, 6, 7, 8, 9, 10, 11] or three-dimensional (3D) electrochemical cells [12, 13, 14, 15]. Thus, under different conditions, zinc and copper electrodeposits yielding needle-like [7, 8, 9, 16, 17, 18], dendrite [6, 7], diffusion-limited aggregation-like patterns (DLA) [5, 6, 7, 9, 10] and a densely branched growth mode (DBM) [6, 7] have been observed.

The formation of branched metal aggregates constitutes an issue of importance from both the fundamental standpoint and their applications. Kinetic data on branched aggregates become interesting to test the validity of and to improve existing growth models. However, the direct comparison of modelling to experimental data and vice versa is often limited by inherent difficulties in the interpretation and poor reproducibility of experiments [4, 5, 6, 7, 8, 9, 10, 12, 13, 14, 15, 16, 17, 18]. On the other hand, branched aggregates are promising microstructural materials with special mechanical properties, although they have deleterious influence on hydrometallurgy and electroplating, causing short circuits in the electrochemical cells and poor quality electrodeposits.

This work describes the growth mode of silver electrodeposition that starts on a platinum cathode from silver sulfate-containing aqueous solutions, in the absence of supporting electrolyte, using quasi-2D electrochemical cells. The influence of silver salt concentration

Dedicated to Prof. Dr. Wolf Vielstich on the occasion of his 80th birthday in recognition of his numerous contributions to interfacial electrochemistry

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in the solution (c_0) , the potential at the cathode (ΔE_c) , the contribution of different mass transport processes and current distribution at different characteristic lengths and growth modes are considered. Pattern morphologies covering from dense to open branching, including dendrites and needle-like formations, can be observed. Rate controlling processes are discussed in terms of dimensionless numbers and current distribution effects.

Experimental

Most of the experiments were run with a quasi-2D cell made of two parallel glass plates and a concentric electrode arrangement consisting of a cathode, made from a piece of platinum wire (99.99%, radius, $r_0=0.035$ cm), and a silver ring anode (radius, $r_a=5.00$ cm, and thickness, $l^2=0.02$ cm) (Fig. 1a). The thickness of the cell was in the range 0.03 cm $\le h \le 0.05$ cm. A silver wire immersed in the same solution, connected to the cell through a capillary tip located at the upper glass plate, was used as the reference electrode. The cell design assured, at least initially, a homogeneous primary current distribution. The cell was placed on a horizontally suspended table to avoid mechanical vibrations [11].

[11]. Working solutions consisted of aqueous silver sulfate $(10^{-3} \text{ M} \le c_0 \le 2.4 \times 10^{-2} \text{ M})$, prepared from Milli-Q* water and analytical reagent-grade chemicals. Prior to filling the electro-chemical cell, solutions were saturated with purified nitrogen for



2 h. The cathode-to-anode and the cathode-reference-electrode ohmic drops were determined by conventional conductometry.

Polarization curves were recorded at potential scan rates (v) in the range $0.001 \le v \le 0.100$ V/s. Silver aggregates were grown in the range 0.38 V $\le \Delta E_c \le 0.80$ V, keeping the cathodic polarization (ΔE_c) constant with respect to the reference electrode.

For each growing electrodeposit, a sequence of photographs at a different time (t) was taken, and simultaneously the cathodic current (I) and the cathodic charge (Q) transients were recorded. Two main sets of transients were obtained. In one of them (data set A), $\Delta E_c = 0.68$ V and c_0 was changed as mentioned above; in another (data set B), $c_0 = 2.4 \times 10^{-2}$ M and ΔE_c varied as already indicated. For both sets A and B, repetitive runs were made to establish the reproducibility of data. Further morphological details of the silver electrodeposits were obtained from scanning electron micrographs.

Results

Polarization curves

A typical polarization curve of silver electrodeposition recorded at v = 0.05 V/s starting from a platinum cathode is shown in Fig. 2. In a cell with a radially growing cathode the current seldom attains a constant value because the cathodic surface area (S) varies continuously with the electrolysis time (t) [19]. This situation turns out to be more complicated when branched electrodeposits are formed.

The first part of theses curves tends to reach an ionic mass-transfer-limited current over a potential range that decreases with v. Beyond this potential range, an increase in current with ΔE_c due to the increase in S can be seen.

For recording current and charge transients the values of ΔE_c were chosen from polarization curves, considering the range of potential where the electrochemical



Fig. 1 (a) Scheme of the quasi-2D cylindrical cell (cell I) used for the electrodeposition of silver. WE=working electrode; CE= counter electrode; RE=reference electrode. (b) Scheme of the quasi-2D cylindrical cell (cell II) used for the determination of the Ohmic resistance with a central "star-like" electrode. H=holding clamp sites

Fig. 2 Typical polarization curve for the electrodeposition of silver on platinum from aqueous 0.024 M silver sulfate using cell I. S=0.223 cm²; v=0.05 V/s; 298 K. Arrows indicate the values of ΔE_c used in this work

reaction is under ionic mass-transfer rate control (Fig. 2).

Determination of cell resistance

Owing to the relatively large cathode-to-anode distance $(d_{\rm ac})$ and the small height (h) of the cell without a supporting electrolyte (small specific conductivity), the ohmic resistance (R_{Ω}) is large. Therefore, it was necessary to determine its value in order to evaluate the ohmic overpotential (η_{Ω}) . The value of R_{Ω} was determined by conductometry and calculated from Ohm's law for a concentrically electrode arrangement:

$$R_{\Omega} = (2\pi h\kappa)^{-1} \ln(r_{\rm a}/r_{\rm w}) \tag{1}$$

where r_a is the inner radius of the ring anode, r_w is the radius of the cylindrical working electrode and κ is the specific conductivity of the solution (Fig. 3). For t=0, $r_w=r_0$.

For irregular electrodeposits, the validity of Eq. 1 was verified using mummy cells provided with starshaped cathodes (Fig. 2b). These electrodes could approximately be described as cylinders of h = 0.05 cm and radius equal to that of the smallest circumference circumscribing the working electrode. Likewise, values of R_{Ω} from the cell with silver branched cathodes of different size and shape were also determined (Fig. 3). In this case, for $r_m < 1.5$ cm, r_m being the greatest outer radius of the electrodeposit, the agreement between experimental data and Eq. 1 was reasonably good.



Fig. 3 Ohmic resistance (R_{Ω}) versus $r_{\rm m}$ plot. *Open circles*: data from different electrodeposits as described in the text. *Large squares*: data from cell II. *Small squares*: data from Eq. 1 for $c_0 = 2.4 \times 10^{-2}$ M and $\kappa = 4.83 \times 10^{-3} \Omega^{-1}$ cm⁻¹ at 298 K, and h = 0.05 cm

Conversely, for $r_{\rm m} > 1.5$ cm, the irregularity of the electrodeposits becomes sufficiently large so that experimental values of R_{Ω} exceed the predictions of Eq. 1. These results show that the true value of η_{Ω} depends on the size and shape of the silver electrodeposits.

Morphology of silver electrodeposits

Silver electrodeposition on platinum at potentials far from equilibrium involves first a nucleation and growth of a thin compact layer [15]. Afterwards, as t and the size of the electrodeposit increase, the development of different types of branching, depending on c_0 , ΔE_c and t, can be seen (Figs. 4 and 5). Generally, these branched patterns can be described as either dense (type I), open (type II), dendrite (type III) or needle-like (type IV). Branching of types I and II shows tip splitting.

Photographs of silver electrodeposits resulting from data set A for $\Delta E_c = 0.68$ V and variable c_0 (Fig. 4a, b) show that the type of branching depends on c_0 and t. For $c_0 = 2.5 \times 10^{-3}$ M (Fig. 4a), branching of types I and III dominates the growth pattern. For $c_0 \ge 1.4 \times 10^{-2}$ M (Fig. 4b), the patterns show branching of types II and III with a small lateral secondary branching.

Photographs of silver electrodeposits resulting from data set B for $c_0 = 2.4 \times 10^{-2}$ M and variable ΔE_c



Fig. 4 Photographs showing the influence of c_0 on the shape of the silver electrodeposits from aqueous silver sulfate grown at $\Delta E_c = 0.680$ V: (**a**) $c_0 = 2.5 \times 10^{-3}$ M; (**b**) $c_0 = 2.4 \times 10^{-2}$ M; 298 K; *reference bar* 1 cm

Fig. 5 Photographs of silver electrodeposits produced from aqueous 0.024 M silver sulfate: (a) $\Delta E_c = 0.38$ V; (b) $\Delta E_c = 0.48$ V; (c) $\Delta E_c = 0.58$ V; (d) $\Delta E_c = 0.68$ V; (e) $\Delta E_c = 0.80$ V; 298 K; reference bar 1 cm



(Fig. 5a–e) also show different types of branching that depend on ΔE_c and t. For $\Delta E_c = 0.38$ V, branching starts on certain sites of the thin compact deposit initially formed. At this potential a single needle tends to dominate the growth pattern (Fig. 5a). For $\Delta E_c = 0.48$ V (Fig. 5b), thick and large branches of type III decorated by a small branching are produced. The number of zigzag-decorated silver branches tends to increase with ΔE_c (Fig. 5c, d). In this case, most segments of large branches tend to form 30° multiple angles. For $\Delta E_c = 0.80$ V, open branching (type II) tends to dominate the growth pattern (Fig. 5e). These patterns also confirm that some branches grow continuously, while the tips of others become thicker and their longitudinal growth rate practically decreases to zero (Fig. 6).

Current transients

In general, most current transients (Fig. 7), which are related to the formation of silver electrodeposits depicted in Figs. 4 and 5, exhibit a complex functionality that correlates with the shape evolution of the electrodeposits in terms of size (r_m) and morphology. For $r_m > r_0$, both *I* and r_m increase continuously as branching

is produced. The slope $\Delta I/\Delta t$ depends on the type of branching, i.e. on the density number of branches and branching growth-rate distribution. Only for a single needle the slope $\Delta I/\Delta t$ remains almost constant. In all cases, branching appears at random at different electrodeposit surface sites either at early stages $(t \rightarrow 0)$ or after a certain time that depends on ΔE_c and c_0 .

Dimension of branched electrodeposits

As c_0 is increased, growth patterns (data set A, Fig. 4) tend to change from dense to open branching. Otherwise, as ΔE_c is increased, growth patterns (data set B, Fig. 5) tend to change from needle-like to open branching and dendrites.

The geometry characterization of global electrodeposits (either data set A or B) was made from the following relationship [1, 2, 3]:

$$Q \propto r_{\rm m}^{D_{\rm M}}$$
 (2)

Then the dimension $(D_{\rm M})$ resulting from the log Q versus log $r_{\rm m}$ plot is $D_{\rm M} \approx 1.6$, i.e. a fractal dimension $(D_{\rm F})$, for the range 10^{-3} M $\leq c_0 \leq 2.4 \times 10^{-2}$ M (Fig. 8a). Similarly, for constant c_0 , $D_{\rm M} = 1.7 \pm 0.1$ for the range 0.48 V \leq





Fig. 7 Current transients for silver electrodeposition from aqueous silver sulfate at 298 K: (a) $\Delta E_c = 0.68$ V; (b) $c_0 = 0.024$ M

Fig. 6 Sequential photographs of a branched electrodeposit grown from 0.024 M aqueous silver sulfate at $\Delta E_c = 0.58$ V: (**a**) t = 2400 s, Q = 0.60 C; (**b**) t = 6960 s, Q = 2.28 C; (**c**) t = 12,360 s, Q = 4.67 C; (**d**) t = 21,480 s, Q = 9.31 C; *reference bar* 1 cm

 $\Delta E_{\rm c} \leq 0.68$ V (Fig. 8b). This value of $D_{\rm M}$ is close to the fractal dimension that has been derived from a DLA growth model and dendritic patterns ($D_{\rm F} \rightarrow 1.71$) [1, 2, 3]. On the other hand, a single needle tip resulting in $\Delta E_{\rm c} = 0.38$ V and low c_0 (Fig. 5a) behaves as an object with an Euclidean dimension ($D_{\rm E}$), i.e. $D_{\rm M} = D_{\rm E} = 1$.

The values of $D_{\rm M}$ were obtained from 35 sets of data resulting from growth patterns of experiments repeated at least twice.

Directional growth rates of branched electrodeposits

The average longitudinal (v_r) and transversal (v_w) growth velocities of each branch were determined. From growth

patterns produced at $c_0 = 2.4 \times 10^{-2}$ M and $\Delta E_c = 0.38$ V, the needle-like branch consists of a ca. 0.2 mm diameter rod-like stem with a sharp tip (Fig. 5a). It appears that out of the various small nodules that can be seen at the stem basis, only the tip with the smallest radius of curvature (r_t) maintains its shape as its growing front continuously displaces. Conversely, branching centres at nodules can also be formed during growth.

Runs at $c_0 = 2.4 \times 10^{-2}$ M and $\Delta E_c = 0.58$ V (Fig. 6a–d) show that some branches, particularly those with a rather thick tip, become practically "dead" branches, although they continue to grow slowly to produce local compact domains.

Average data for v_r and v_w from a single branch, calculated from magnified patterns at different ΔE_c , c_0 and t_d , are assembled in Table 1. The number of hindered-growth branches increases with c_0 and decreases with ΔE_c . The $\langle v_r \rangle / \langle v_w \rangle$ ratio is in the order of 10²,

irrespective of c_0 and ΔE_c . This figure is consistent with data derived for gold dendrite electroformation on highly oriented pyrolytic graphite [20].

Discussion

General considerations for silver electrodeposition from a binary electrolyte

Silver ion electrodeposition on silver from silver-ioncontaining aqueous solution can be represented by the following reversible reaction:



Fig. 8 (a) $D_{\rm M}$ versus c_0 plot; $\Delta E_{\rm c} = 0.68$ V. (b) $D_{\rm M}$ versus $\Delta E_{\rm c}$ plot; 0.024 M aqueous silver sulfate; 298 K

 $Ag^+(aq) + e^-(cathode) \longrightarrow Ag^+(crystal)$ $+ e^{-}$ (conduction band) (3)

The equilibrium potential (E_r) of reaction (3) is given by the Nernst equation:

$$E_{\rm r}({\rm Vvs.SHE}, 298{\rm K}) = 0.799 + 0.059 \log(a_{\rm i}/a_0)$$
 (4)

where a_i and a_0 are the activity of silver ions in the solution and solid silver, respectively, the latter being taken equal to 1.

The kinetics of reaction (3) is strongly dependent upon the crystallographic faces, their distribution and the existence of surface defects [21, 22, 23, 24, 25]. Thus, for stepped polycrystalline silver surfaces, the exchange current density at 298 K is $j_0 = 24 \pm 5$ A/cm² for $c_0 = 1$ M [22]. Accordingly, on these electrode surfaces, reaction (3) can be considered as one of the fastest, most electrochemically reversible interfacial processes. Then, under conventional electrodeposition conditions such as those used in this work, the global kinetics of reaction (3) is under ionic mass-transfer rate control. Therefore, the steady flux of depositing ions (i) towards the electrode surface can be expressed by the convective diffusion equation [26, 27]:

$$\mathbf{N}_{\mathbf{i}} = D_{\mathbf{i}} \nabla c_{\mathbf{i}} - \mathbf{V} c_{\mathbf{i}} + z_{\mathbf{i}} u_{\mathbf{i}} c_{\mathbf{i}} F \nabla \phi \tag{5}$$

where N_i is the mass transfer flux vector for depositing i ions, $D_{\rm i}$, the corresponding diffusion coefficient, V the fluid velocity vector, ϕ the single electrode potential and u_i the i-ion mobility. Considering the electroneutrality condition and a simple cell geometry, the solution of Eq. 5 leads to a current density equation formally similar to that derived either in the presence of a supporting electrolyte or for a binary electrolyte provided that the solution diffusion coefficient (D_s) rather than the diffusion coefficient of each reacting ion (D_i) is used in the flux equation. The relationship between D_s and D_i is [26, 27]:

$$D_{\rm s} = D_{-}D_{+}(z_{+} - z_{-})/(z_{+}D_{+} - z_{-}D_{-})$$
(6)

where z_+ , z_- and D_+ , D_- denote the charge and the diffusion coefficient of cations (+) and anions (-), respectively.

Let us consider dimensionless numbers to estimate the different contributions to ionic mass-transfer-controlled silver electrodeposition [28, 29]. The Péclet

$\Delta E_{\rm c}$ (V)	Range of $t (10^3 s)$	Range of $Q(C/cm^2)$	Total number of branches	Number of "dead" branches	$< v_r > x 10^4$ (cm/s)	$< v_{\rm w} > x 10^6$ (cm/s)		
0.024 M Ag ₂ SO ₄								
0.38	5.4-9.12	0.92 - 1.74	9	8	1.2 ± 0.8	3 ± 1		
0.58	2.4-21.5	0.60-9.31	8	3	0.8 ± 0.2	0.7 ± 0.3		
0.68	1.2-16.2	0.34-9.64	7	1	1.1 ± 0.2	0.7 ± 0.4		
0.010 M	Ag ₂ SO ₄							
0.68	1.68-11.5	0.21-2.59	6	4	1.4 ± 0.3	2 ± 1		
	$ \frac{\Delta E_{\rm c} (\rm V)}{0.024 \rm M} \\ 0.38 \\ 0.58 \\ 0.68 \\ 0.010 \rm M \\ 0.68 $	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$	$\begin{tabular}{ c c c c c c c c c c c c c c c c c c c$		

number (Pe) indicates whether the rate of displacement of the growing front becomes sufficiently high to produce forced convection, whereas the Rayleigh number (Ra) is an indication of the contribution of free convection. Pe results from the product of the Reynolds (Re) and Schmidt (Sc) numbers [26, 30]:

$$Pe = Re \times Sc = \delta_h / \delta_d = Lv_r / 2D_s$$
(7)

where δ_h and δ_d are the thickness of the hydrodynamic and mass-transfer boundary layer, respectively, *L* is the characteristic length of the system, and v_r is the displacement rate of the growth front. The Rayleigh (Ra) number is the product of the Grashof (Gr) and Schmidt (Sc) numbers:

$$Ra = Gr \times Sc = g\alpha L^3 / \nu D_s \tag{8}$$

where g is the gravity constant, v the cinematic viscosity of the solution and α the densification coefficient, defined as [26]:

$$\alpha = (c_0/\rho_0)(\partial \rho/\partial c) \tag{9}$$

where ρ^0 and ρ are the specific gravity in the bulk of the solution and in the diffusion layer, respectively. The same subscripts are applied to the concentration terms.

Values of Pe and Ra calculated from Eqs. 7 and 8 for different growth patterns (Figs. 4 and 5) are assembled in Table 2, where data used for the calculations are also included. For isolated branch tips (Fig. 5a) we consider $L=r_t$, the value of r_t being determined from SEM micrographs (Fig. 9), whereas for global branched patterns we considered either $L=r_m$ or L=h. Data indicate that for the growth of both silver single tips and branched patterns the influence of forced convection can be disregarded. For isolated tips, Ra < 31, 32].

Contributions to the growth of branched patterns

The change in the shape of the deposit from cylindrical to irregularly branched along the process indicates that the initially axially symmetric current distribution changes to an arbitrarily non-uniform one due to the influence of local concentration fluctuations at the

Table 2 Dimensionless numbers calculated for single tips and ramified silver electrodeposits (aqueous 0.024 M silver sulfate, 298 K)^a

Morphology type	L (cm)	$< v_r > (cm/s)$	Pe	Ra
Tip	0.004	6×10 ⁻⁵	1.2×10^{-2}	_
Tip	0.01	2.3×10^{-4}	1.9×10^{-2}	9.8×10^{-1}
Branching	0.035	1×10^{-4}	1.75×10^{-1}	-
Branching	4	6×10^{-4}	1.20×10^2	_
Branching	0.03	_	_	2.7×10^{1}
Branching	0.05	_	-	1.25×10^{2}
Dranching	0.05	—	_	1.23×1

^aFirst row data: $L=r_t$. Second row data: $L=r_t$. Third row data: $L=r_0$. Fourth row data: $L=r_m$. Fifth and sixth rows data: L=h. Values of $\alpha = 0.01$, $\nu = 0.01$ cm²/s and $D_s = 1.2 \times 10^{-5}$ cm²/s at 298 K were taken from [26, 27, 29]

electrodeposit surface. Local concentration fluctuations trigger the growth of local irregularities as the nucleation of depositing atoms is involved in the electrocrystallization of metals. The formation of new nuclei requires a certain overpotential that is a part of the electrocrystallization overpotential, but once nuclei are formed the latter decreases and the current density on the newly formed small crystals increases. Subsequently, the attachment of depositing atoms onto the lattice occurs preferentially at step sites or protrusions where there is an increase in the average current density.

On the other hand, for an ionic mass-transfer-controlled process, such as silver electrodeposition on a platinum substrate, branching triggering occurs after a first compact silver thin layer is formed on the substrate [15]. Accordingly, as the number of irregularities begins to increase, a non-homogeneous current microdistribution profile sets in. Then, let us compare the value of δ_d to the branch tip separation (*L*'). In fact, δ_d varies from an initially uniform value around the cylindrical cathode ($L' < \delta_d$) to different local values at the irregularly branched cathode, i.e. small and large values of δ_d at protrusions and valleys, respectively. The average value of δ_d estimated from the ratio $< \delta_d > = D_s/$ $< v_r >$ varies in the range 0.025 $\le < \delta_d > \le 0.20$ cm.

The dense morphology arising for $L > \delta_d$ and $L' < \delta_d$ indicates that all surface sites approach a similar growing probability. In this case, the value of δ_d tends to be independent of the microstructure of the deposit surface. Also in this case, free convection contributes to the transport process, as is concluded from the analysis of dimensionless numbers (see above). Free convection then acting as a local stirring effect assists to produce denser electrodeposits [17]. Accordingly, both surface diffusion and free convection promote correlation effects at protrusions and the development of a fractal surface.

Conversely, for open branched patterns, $L > \delta_d$ and $L' > \delta_d$, as each protrusion will tend to grow separately, and the mass transfer boundary layer will tend to follow the surface contour of the protrusion. The tip growth probability is then largely increased. Recently, it has been established [33] that the smallest value of δ_d at the tip site itself remains constant either for stable or marginally stable tips. In this case, as there is no significant convective contribution at the tip, the rate of mass transfer is mainly determined by the hemispherical diffusion of reactants to the tip surface [34]. Accordingly, the compensation between the high current density at tips and surface relaxation processes, such as that produced by surface adatom diffusion and surface tension effects [1, 2, 3], determines the tip stability. Then, an optimal tip radius is maintained at a maximum growth rate of the deposit [33]. In contrast to dense branching, for non-correlated open branching the value of L' increases along the radial growth of the deposit, turning the current distribution increasingly inhomogeneous. This situation favours the development of open mass fractal domains (Fig. 5c).



Fig. 9 SEM micrograph of a needle tip. Reference bar 100 µm

On the other hand, for dendrites, adatom surface diffusion contributes to both branching thickening and to tip stabilization. Growth patterns depicted in Fig. 6 show a slow uniform branch thickening, although the rate of this process appears to be specific to each branch. Thickening also occurs at the tip of dead branches, leading to a compact quasi-spherical deposit. Silver atom surface diffusion also plays a key role in branch thickening, as in the case of metal dendrite formation [20, 35, 36].

In summary, the growth mode of silver branched electrodeposits in a quasi-2D cell can be described by a complex process involving a competition between phenomena at the macro- and microscopic level promoting the formation of either a compact pattern or irregular patterns, including open and dense branching. The relative contribution of these phenomena depends on c_0 , ΔE_c and t. Correspondingly, current macro- and micro-distributions determine the type of growth mode of the global electrodeposit.

Conclusions

- 1. The electrodeposition of silver from silver sulfate aqueous solutions in a quasi-2D cell, at 298 K, produces complex growth patterns involving dense branching, DLA-type, dendrite and needle-like patterns.
- 2. The dominant morphology depends on c_0 , ΔE_c and t. Under certain conditions the patterns exhibit domains with different morphologies that are irregularly distributed.
- 3. The analysis of dimensionless numbers allowed us to distinguish the ionic mass-transfer mechanism contribution in the electrochemical process.
- 4. The axial-to-radial growth rate ratio of a single branch is close to 10^2 .
- 5. The branch density number increases with $\Delta E_{\rm c}$ and decreases slightly with c_0 .
- 6. The formation of complicated silver patterns can be described by a complex physical mechanism involving a competition between phenomena at the

macroscopic and atomic level promoting the formation of compact or irregular either open or dense branched patterns.

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